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(54) Title: EASY-OPEN PACKAGING

(57) Abstract

A laminate fabricated from a film or a sheet capable of forming peel seals suitable for vertical form/fill/seal packaging, which is made from a blend of an ethylene polymer, a metallocene-made polyethylene and a poly-1-butene polymer.

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DESCRIPTION EASY-OPEN PACKAGING

Technical Field

This invention relates to a heat sealable wrapping or packaging film which is capable of forming a peelable seal having improved hot tack strength for vertical form/fill/seal packaging. Particularly, this invention relates to a film, a sheet or a laminate structure fabricated from a blend of an ethylene polymer made by a conventional catalyst, a metallocene-made polyethylene, and a butene-1 homopolymer or copolymer. The seal is achievable either between two films of this kind or between one film of this kind and a rigid container without the need for an adhesive between this film and the container.

Background Art

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15 A peelable seal is defined to be a seal or joint between two films produced by heat sealing or impulse sealing. The joint thus formed having sufficient peel strength, the property of being able to open in the original plane of joining of the two films by the action of a pulling force, without 20 tearing occurring in the material of the two films used to make For the purposes of the present invention, the up the joint. peelable seal must possess a mechanical resistance (peel strength) sufficient to maintain the wholeness and the tight-seal properties of the packing and wrapping during storage and 25 transport until such time as the packing or wrapping is opened by the user of the article. The mechanical resistance of the peelable seal must be low enough to permit ready manual opening of the joint, i.e., without the use of any auxiliary instrument.

This invention relates to a blend, and a method for making a blend usable in a flexible film package. This invention also relates to a film and/or a laminate which are characterized by a nearly constant peel strength over an extended heat seal temperature range and by being peelable. The term peelable refers to a film having seal failure which occurs primarily at the interface of the sealing surface, and not by film tearing. The blends, films, and/or laminates of the present invention permit the manufacture of a more consistent finished product, having a

seal of predictable and constant peel strength, in spite of inevitable variations in the heat seal temperatur s used in the production of such packages.

In the past, many variations of thermoplastic materials have been employed in the manufacture of films capable of forming peelable seals. Poly-1-butene homopolymer or copolymers, low density polyethylenes made by conventional catalysts, and low density polyethylenes made by metallocene catalysts each has certain hot tack strength. However, each of these polymers by itself exhibits a seal strength which is too strong and thus unsuitable for making peelable seals.

Blends of polyethylene homopolymers or copolymers with poly-1-butene polymers have been used commercially for making horizontal form/fill/peel seals. However, it lacks the required hot tack strength, that is the seal strength at elevated temperatures for vertical packaging. Hot tack strength is a critical property in the vertical form/fill/seal packaging. Vertical form/fill/seal packaging involves first sealing the bottom portion of the packaging films/laminates, such as bags, under an elevated temperature. This is immediately followed by filling the material to be packed, such as food, into the packaging films/laminates such as bags by "gravity", while pushing hot air downwardly into the bags. The top portion of the bag is then sealed with heat. In order to provide sufficient seal strength in vertical form/fill/seal packaging, the polymeric peel seal films must have sufficient seal strength at elevated (hot tack strength) so that the seals would not cemperatures break during a vertical form/fill/seal packaging process.

There has been a long felt need for a blend having the required peel strength for use in peelable packaging seal, while having the required hot tack strength for use in certain applications such as vertical form/fill/seal packaging.

Disclosure of the Invention

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It has now been found that certain properties including hot tack strength may be improved by fabricating films or sheets from blends having (i) 15-85 weight percent of an ethylene polymer made by a conventional catalyst, (ii) from about 10% to

about 70 weight percent of a metalloc ne-made polyethylene and (iii) from about 5 percent by weight to about 55 percent by weight of butene-1 homopolymer or copolymer. Such films or sheets are bonded to a substrate (or backing material) by coextrusion or extrusion lamination.

Brief Description of the Drawing

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The drawing illustrates that the hot tack strengths of the present polymeric blends with LDPE (low density polyethylene made by a conventional Ziegler-Natta Catalyst), PB (poly-1-butene) and mLDPE (low density polyethylene made by a metallocene catalyst) are improved over a blend on LDPE and PB without mLDPE. Detailed Description of the Invention

While the present invention is described in connection with the preferred embodiments, it will be understood that it is not intended to limit the invention to those embodiments. On the contrary, it is intended to cover all alternatives, modifications, and equivalents as may be included within the spirit and scope of the invention as defined by the appended claims.

The present invention is directed to a composition for producing a peelable heat seal film or sheet suitable for vertical form/fill/seal packaging comprising (i) from about 15 wt% to about 85 wt.%, specifically from about 35 wt.% to about 80 wt.%, more specifically from about 55 wt% to about 70 wt.%, of an ethylene polymer made by a conventional catalyst (ii) from about 10 wt.% to about 70 wt.%, specifically from about 20 wt.% to about 50 wt.%, more specifically from about 25 wt.% to about 45 wt.%, of a metallocene-made polyethylene, and (iii) from about 5 wt.% to about 55 wt.%, specifically from about 10 wt.% to about 40 wt.%, more specifically from about 15 wt.% to about 30 wt.% of a butene-1 homopolymer or copolymer. The weight percentages used herein are all based on the total weights of the blends.

The present invention is also directed to a film or a sheet made from the afore-mentioned blend. A film or sheet made from said blend, could be laminated with backing materials (or substrates), sealed to itself or to a rigid container at a heat sealing temperature of between about 160°F and about 500°F, as

determined at sealing jaws, affords a peel strength of between about 0.5 to about 8.0 pounds per inch, specifically from about 1.0 to about 6.0 pounds per inch, more specifically between about 1.5 to about 4.0 pounds per inch between the backing material and a rigid container. A film or a sheet made from said blends also affords a hot tack strength of from about 1.0 about 4.0 newton/15 mm, specifically from about 1.5 to about 3.5 Newton/15 mm, more specifically from about 2.0 to about 3.0 Newton/15 mm.

This invention is also directed to a laminated film, adapted for producing a material for making a container lid and a heat sealing film made from a blend of the above-mentioned composition. The laminated film has utility for achieving at a sealing temperature of about 160°F and about 500°F, as determined at sealing jaws, a peel strength of between about 0.5 to about 8.0 pounds per inch, specifically from about 1.0 to about 6.0 pounds per inch, more specifically between about 1.5 to about 4.0 pounds per inch between the backing material and a rigid container. A film or a sheet made from said blends also affords a hot tack strength of from about 1.0 about 4.0 Newton/15 mm, specifically from about 1.5 to about 3.5 Newton/15 mm, more specifically from about 2.0 to about 3.0 Newton/15 mm.

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The term ethylene polymer made by a conventional catalyst refers to any polyethylene homopolymer, any ethylene- α olefin copolymer, or any ethylene-unsaturated ester copolymer made by a conventional catalyst such as a Ziegler-Natta catalyst. The polyethylene homopolymer or ethylene- α -olefin copolymer is made by a conventional Ziegler-Natta Catalyst of Group IV-VI transition metal, specifically by a vanadium metal compound, a zirconium metal compound or a titanium halide (TiCl, or TiCl3), optionally supported by magnesium halide, with an aluminum trichloride or alkyl aluminum (halides) cocatalyst. Suitable polyethylene include all commercially available ethylene homopolymers, ethylene- α -olefin copolymers, such as a high density polyethylene (HDPE) with density of more than 0.94 g/cc, a medium density polyethylene with density of 0.93 to 0.94 g/cc, a low density polyethylene (LDPE) with density of less than 0.93 g/cc, or a linear low density polyethylene (LLDPE).

specific embodiment of the present invention, the polyethylene is a LDPE, more specifically LDPE 2500 or LDPE 2500FA, which may contain certain additiv s, available from Shell Chemical Company located at London England.

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The ethylene-unsaturated ester copolymer refers to any compolymer made by copolymerizing of ethylene and an unsaturated ester using a conventional catalyst. The unsaturated esters are esters of (i) carboxylic acids having 1-8 carbon atoms, and (2) an alcohol having 2-8 carbon atoms and containing at least one double bond. Non-limiting examples of suitable unsaturated ester include vinyl acetate, vinyl butyrate, vinyl formate, etc. As a specific embodiment of the present invention, the DuPont Alathon® 3159 polyethylene-vinyl acetate is used. These ethyleneunsaturated ester copolymers are polymerized by conventional illustrative An non-limiting example conventional process involves the used of any conventional Ziegler-Natta catalyst(s).

The metallocene-made ethylene polymer referred to herein are any ethylene homopolymer or ethylene- α -olefin copolymer made by a metallocene catalyst. As a specific embodiment of the present invention, the metallocene-made polyethylene is a low density polyethylene, more specifically a copolymer of ethylene with an alpha olefin comonomer having from 4-12 carbon atom. As a more specific embodiment of the present invention, a ethylene/1-octene copolymer(s), ethylene/1propene/1-octene terpolymer(s), and mixture thereof, made by a metallocene catalyst is used. As a still more specific embodiment of the present invention, a metallocene-made low density polyethylene purchased from Dow Chemical identified as Affinity FM 1570, which is an ethylene-octene copolymer, is used as the parent thermoplastic. As another still more specific embodiment of the present invention, a metallocenemade low density polyethylene purchased from Dow Chemical Company identified as Affinity PL 1850, which is an ethylene-octene copolymer, is used as the metallocene-made low density polyethylene.

Metallocene catalysts, also referred to as constrained geometry catalysts, are characterized as having a singl , stable chemical type rather than a volatile mixture of states as discussed for conventional Ziegler-Natta catalysts. This results in a system composed of catalyst positions which have a singular activity and selectivity. For this reason, metallocene catalyst systems are often referred to as "single site" owing to the homogeneous nature of them, and polymers and copolymers produced from them are often referred to as single site resins by their suppliers.

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Generally speaking, metallocene catalysts organometallic compounds comprising a metal coordination complex comprising a metal of groups 3-10 or the Lanthanide series of the Periodic Table of the Elements, preferably a metal of groups 3-6, and especially a metal of groups 4 and 5, such as hafnium, titanium, vanadium, or zirconium, and a delocalized pi-bonded moiety substituted with a constrain-inducing moiety, such as one or more cyclopentadienyl ligands. A cocatalyst, such as but not limited to, oligometric methyl alumoxane is often used to promote the catalytic activity. By varying the metal component and the cyclopentadienyl ligand a diversity of polymer products may be tailored having molecular weights ranging from about 200 to greater than 1,000,000 and molecular weight distribution from 1.5 to about 15. The choice of co-catalyst influences the efficiency and thus the production rate, yield, and cost.

Exxon Chemical in U.S. Patent 4,701,432 sets out examples of which olefin catalyst systems are of the metallocene which are non-metallocene. They bis(cyclopentadienyl) dichloro-transition metal, bus(cyclopentadienyl)methyl, chloro-transition metal, bis(cyclopentadienyl)dimethyl-transition metal as examples of metallocene catalysts, where the metals include choices such as titanium, zirconium hafnium, and vanadium. The patent further provides examples of non-metallocene catalysts as being TiCl4, TiBr₄, Ti(OC_4H_9)₂Cl₂, VC₁₄, and VOCl₃.

As a consequence of the single site system afforded by metallocenes, olefinic copolymers, such as ethylene/alpha-olefin

copolymers, can be produced with each polymer chain having virtually the same architecture. Therefore, the copolymer chains produc d from single site systems are uniform not only in chain length, but also in average comonomer content, and even regularity of comonomer spacing, or incorporation along the chain.

In contrast to Ziegler-Natta catalyst made polymers, these single site metallocene polymers are characterized as having a narrow MWD and narrow compositional distribution (CD). While conventional polymers have MWD's of about 3.5 to 8.0, metallocene-made polymers range in MWD from about 1.5 to about 2.5 and most typically about 2.0. MWD refers to the breadth of the distribution of molecular weights of the polymer chains, and is a value which is obtained by dividing the number-average molecular weight into the weight-average molecular weight. low CD, or regularity of side branches chains along a single chain and its parity in the distribution and length of all other chains, greatly reduces the low MW and high MW "tails". These features reduce the extractables which arise from poor LMW control as well as improve the optics by removing the, e.g. linear, ethylene-rich portions which are present in conventional heterogeneous resins.

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Thus, conventional Ziegler-Natta systems produce heterogeneous resins which reflect the differential character of their multiple catalyst sites while metallocene systems yield homogeneous resins which, in turn, reflect the character of their single catalytic site.

Another distinguishing property of single site catalyzed ethylene copolymers is manifested in their melting point range. The narrow CD of metallocenes produces a narrow melting point range as well as a lower Differential Scanning Calorimeter (DSC) peak melting point peak. Unlike conventional resins which retain a high-melting point over a wide density range, metallocene resin melting point is directly related to density. For example, an ethylene/butene-1 copolymer having a density of 0.905 g/cc produced using a metallocene catalyst has a peak melting point of about 100°C, while a slightly lower

density ethylene/butylene copolymer which was made using a conventional Ziegler catalyst reflects its heterogeneous nature with a melting point at about 120°C. DSC shows that the Ziegler resin is associated with a much wider melting point range and actually melts at higher temperatures despite its lower density.

In recent years, several resin suppliers have been researching and developing metallocene catalyst technology. The following are patent literature disclosing none-limiting illustrative examples of metallocene catalysts which are suitable for use in preparing the thermoplastics of the present invention and processes of preparing metallocene-made thermoplastics, the teaching of which are incorporated herein by reference.

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Dow in EP 416,815 disclosed the preparation of ethylene/olefin copolymers using monocyclopentadienylsilane complexed of a transition metal. The homogeneous ethylene copolymers which may be prepared using this catalyst are said to have better optical properties than typical ethylene polymers and be well suited for film or injection molding.

Wellborn in Exxon U.S. 4,306,041 discloses the use of metallocene catalysts to produce ethylene copolymers which have narrow molecular weight distributions.

Chang, in Exxon U.S. 5,088,228 discloses the production of ethylene copolymers of 1-propene, 1-butene, 1-hexene, and 1-octene using metallocene catalysts.

Exxon in U.S. 4,935,397 discloses the production of ethylene copolymers using metallocene catalysts to manufacture polymer suitable for injection molding or thermoforming.

Wellborn, in Exxon U.S. 5,084,534 discloses the use of bis(n-butylcyclopentadienyl)zirconium dichloride to produce high molecular weight polyethylene having a polydispersity of 0.8 and a density of 0.955/cc.

In Exxon U.S. 3,161,629 a cyclopentadienyl complex is disclosed which may be used to produce polyolefins having controlled molecular weight and density suitable for use in extrusion of injection molding.

Canich in Exxon U.S. 5,055,438 and 5,057,475 discloses the use of mono-cylcopentadienyl catalysts having a unique

silicon bridge which may be employed to select the stereochemical structure of the polymer. Catalysts such as methyl, ph nyl, silyl, tetramethylcyclopentadienyl-terbutylamidozirconium dichloride may be used to produce polyethylene and ethylene copolymers suitable for films and fibers.

Mitsui Toatsu in JP 63/175004 employed bis(cylcopenta-dienyl)ethoxy-ZrCl to prepare homogeneous ethylene copolymers.

Mitsubishi in JP 1,101,315 discloses the use of bis(cyclopentadienyl) $\rm ZrCl_2$ for the preparation of ethylene butene copolymers.

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Dow Chemical in WO 93/13143 discloses an ethylene/alpha-olefin interpolymer products comprising a first homogeneous ethylene polymer, specifically a copolymer of ethylene and 1-octene, made with a titanium metallocene catalyst and a second homogeneous ethylene/alpha-olefin copolymer, specifically a copolymer of ethylene and 1-octene, made with a zirconium metallocene catalyst.

As one specific embodiment of the present invention, the metallocene-made polyethylenes are polyethylenes produced by polymerizing ethylene with an alpha-olefin having from 4 to 12 carbon atoms, optionally one or more other alpha-olefin(s) having from 3 to 12 carbon atoms, in the presence of metallocene catalysts which achieve a density from 0.860 to 0.930, particularly from about 0.860 to about 0.920, a molecular weight distribution of less than 4, particularly less than 3, and good distribution of ethylene and from about 0% to about 40%, particularly from about 8% to about 30%, by weight of an alphaolefin comonomer having from 4 to 12 carbon atoms, and optionally from about 0% to about 40% by weight of one or more other alphaolefin(s) having from 3 to 12 carbon atoms such as propylene. The metallocene-made polyolefins are produced as described in U.S. Patent Nos. 5,322,728 and 5,272,236 which descriptions are incorporated by reference herein. Such metallocene polyolefins are available from Dow Chemical Company under the trademarks ENGAGE and AFFINITY (ethylene/octene copolymers) and from EXXON Chemical Company under the trademark EXACT (ethylene/butene copolymers).

The polymerization process for making the metallocenemade thermoplastics may be accomplished, although not limited to, at conditions well known in the prior art for Ziegler-Natta r Kaminsky-Sinn type polymerization reactions, that is, temperatures from 0 to 250°C and pressures from atmospheric to 1000 atmospheres (100 MPa). Suspension, solution, slurry, gas phase or other process conditions may be employed if desired. A support may be employed but preferably the catalysts are used in a homogeneous manner. It will, of course, be appreciated that the active catalyst system, especially nonionic catalysts, form in situ if the catalyst and the cocatalyst components thereof are added directly to the polymerization process and a suitable solvent or diluent, including condensed monomer, is used in said polymerization process. It is, however, preferred to form the active catalyst in a separate step in a suitable solvent prior to adding the same to the polymerization mixture.

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The metallocene-made thermoplastic polymers usable herein can be either homopolymers or copolymers. If copolymers are used, they can be binary copolymers, ternary copolymers or terpolymers, or copolymers with 4 or more monomers; they can be random or block copolymers. As a specific embodiment of the present invention, polyethylene useful in the present invention have a melt index of less than 60, more specifically from about 0.1-15, as measured by ASTM D-1238, condition E at 190°C.

Metallocenes make polymers with uniform, narrow molecular weight distribution (MWD), high comonomer content, relatively even comonomer distribution and an enormously wide choice of comonomers, compared to multi-site Ziegler-Natta catalysts.

The poly-1-butene usable herein is a homopolymer or copolymer containing more than 50 mole% butene-1 having a melt index of from about 0.05 to about 300, specifically from about 0.1 to about 40, and more specifically from about 0.4 to about 10 dg/min., as determined by ASTM D-1238 condition E, at 190°C.

As a specific embodiment of the present invention, the polybutylene referred to herein is a butene-1 polymer containing from 90% preferably from 95% and more preferably from 97% by

weight of stereospecific portions. These stereospecific portions can be either isotactic or syndiotactic. As an illustrative example, isotactic poly-1 butenes having a low molecular weight, e.g. about 280,000 as determined by solution viscosity in "Decalin" (decahydronaphthalene) may be used. A butene-1 polymer (PB) usable herein is either a butene-1 homopolymer or a copolymer or a terpolymer. If a butene-1 copolymer is used, the non-butene comonomer content is from 1 to 50%, preferably from 1 to 30 mole% of either ethylene, propylene, or an alpha olefin having from 5 to 8 carbon atoms. The poly-1-butenes can be modified to increase surface activity by reaction with, for example, maleic anhydride.

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Suitable poly-1-butenes can be obtained in accordance with polymerization of butene-1 with catalysts of halides of IV-VI metals, e.g. titanium, vanadium, chromium, zirconium, molybdenum and tungsten, etc. and cocatalysts of metal alkyl compounds, specifically, Ziegler-Natta catalysts of titanium halides or vanadium halides with aluminum halides or aluminum alkyl (halides) compounds. As a specific examples, the poly-1-butene can be obtained by a low-pressure polymerization of butene-1, e.g. by polymerizing butene-1 with catalysts of TiCl3 or TiCl₃-AlCl₃ and Al(C₂H₅)₂Cl at temperatures of 10-100°C, preferably 20-40°C, or TiCl₃-AlCl₃ and Al(C₂H₅)₂Cl at temperatures of 10-100°C, preferably 20-40°C, e.g. according to the process described in DE-A-1,570,353 or U.S. Pat. No. 3,197,452. High melt indices are obtainable by further processing the polymer by peroxide cracking, thermal treatment or irradiation to induce scissions leading to a higher melt flow material.

Suitable poly-1-butenes can also be obtained using a high activity Ziegler-Natta catalyst of magnesium supported TiCl₄, with organoaluminum or AlCl₃ cocatalyst. It can be polymerized by a gas phase, liquid phase, suspension, solution phase, or slurry polymerization process.

Duraflex® PB 0110, a polybutylene polymer produced by Shell Chemical Company, of Houston, Texas is a particularly suitable polymer. This polymer is a homopolymer with a melt

index of 0.4 g/10 min. at 190° C and a molecular weight of about 800.000.

A preferred blend uses about 15-25 wt% of a butene-1 polymer having a melt index equal to 0.4-10 dg/min. (ASTM 1238 condition E), and 20-45 wt% of a metallocene-made polyethylene, e.g. an low density ethylene-octene copolymer such as Affinity PL1850, and 55-70 wt% LDPE of such as LDPE 2500 or LDPE 2500 FA.

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Blending of the components can occur by, for example, dry tumble blending, masterbatch, or melt compounding techniques. The method of combining the ingredients of the formulation is important. For example, in most cases, it is desirable to use the least amount of energy to merge the components into an effective blend. Therefore, the preferred method of blending is dry blending the component.

The novel polymer mixtures may be formed into an oriented or unoriented film by casting or film blowing method. After fabrication, the film can be heat sealed by sealing jaws at a preset temperature, pressure, and dwell. The seal strength is tested by an Instron tensile tester at 10"/min. crosshead speed. Maximum strength on a one inch width strip was designated as peel seal strength.

These manufacturing techniques are applicable to film making, although this invention may also be applied to sheet making. Films refer to shaped plastics that are comparatively thin and have maximum thickness of about 0.010 inches (10 mils). Sheets are shaped plastics having thickness greater than 0.010 inches.

The present invention also relates to the peel seal coating layer of a laminated structure comprising a backing material and said peel seal coating. The peel seal coating, which consists of a blend of the present invention can be coated or laminated onto a desired backing material. The backing material can be a member of the group consisting of, but not high poly-4-methyl pentene, nylon, limited to polystyrene, foil, polycarbonate, aluminum polyethylene, polyurethane, polyvinyl chloride, polyester, polyacrylonitrile, and polypropylene. Except for high density polyethyl ne, nylon

and the aluminum foil, the remaining backing material may requir a tie layer adhesive for use with the novel film layer.

The laminated structure can be made by making two separate films that are then laminated. The films may be prefabricated by either film blowing (melt extrusion with a circular die) or the casting method (a flat die-melt extrusion process).

The resultant film article can be prepared by any suitable means, such as heat lamination or coextrusion. Coextrusion techniques that can be used for the preparation of the instant film include those described in details in U.S. Pat. No. 2,480,998.

Melt extrusion with a flat die (casting) may be accomplished for the present blends by using a flat die or slot The extrusion process starts with the present blends in a form that can be fed continuously into an extruder by means of a screw or pneumatic tube. Sometimes, the polymers are combined with materials such as plasticizers, lubricants, (anti-)slip agents, anti-blocking agents, stabilizers, and colorants by means The resulting mix is extruded through rod of Banbury mixers. shaped dies and chipped into pellets. Pelletized polymer is fed into a screw conveyor into the end of screw-type extruder and is heated and made into viscous fluid in a cylinder by means of a The sheet emitting from the die is revolving, helical screw. quenched on a temperature controlled chill roll. Finished films may be subject to a two-way stretching using continuous tenterframe operation in biaxial orientation.

As used herein, the word "comprises" means "including the following elements but not excluding others."

The invention will be illustrated by the following illustrative embodiments which are provided for illustration purpose only and are not intended to limit the scope of the instant invention.

ILLUSTRATIVE EMBODIMENT I

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Blends were prepared by dry blending in a tumbler mixer the following three ingredients; (i) LDPE 2500 or LDPE 2500FA available from Shell Chemical Company in London, England; (ii)

Affinity PL1845, an ethylene-octene copolymer of a density of about .910 gm/cc (ASTM D-1238) made by metallocene, available from Dow Chemical Company, and (iii) Duraflex® PB0110 poly-1butene homopolymer, available from Shell Chemical Company, Houston, Texas, having a melt index of about 0.4 dg/min. (ASTM method D-1238 condition "E") and a density of about 0.9. resultant blends were each coextruded with Hoechst-Celanese 7740 high density polyethylene (HDPE) at a die temperature of about 210°C. into films of about 2.5 mils in thickness using a flat die. The films each comprised 2.0 mils of HDPE and 0.5 mils of the remaining components. Hot tack strengths were tested. Film samples of each composition of one inch wide and 12 inches long were tested at temperatures of 90, 100, 110, 120 and 130 °C. Hot tack strengths were determined using a DTC Hot Tack Tester using 40 psi seal bar pressure, 150 mm/sec peel speed, 0.5 seconds dwell time and 0.3 seconds delay time setting. Hot tack strengths for the films, and the compositions of the films are provided in TABLE I.

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	TABLE 1				
HOT TACK STREN	GTH OF PB-	-LDPE-mLD	PE BLENDS	<u> </u>	
Blends Compositions		Hot Tack	Strength	(N/INCH)	
Sealing Temperature, °C	90	100	110	120	130
80% LDPE + 20% PB (Control)	0.16	0.359	0.955	0.739	0.7
60% LDPE + 20% PB + 20% mLDPE	0.141	0.408	1.478	1.199	2.245
40% LDPE + 20% PB + 40% mLDPE	0.233	1.203	2.861	2.652	2.814
20% LDPE + 20% PB + 60% mLDPE	0.164	1.697	2,956	2.924	2

As may be seen from TABLE 1, the films made from various blends of the present invention and the control blend(PB and LDPE) were tested for hot tack strength in Newtons per inch at sealing temperatures of 90, 100. 110, 120, and 130°C. It has been unexpectedly found that the addition of a metallocene-made polyethylene, specifically AFFINITY PL 1845 (an ethylene-octene low density copolymer made by metallocene), to a blend of polybutylene and LDPE (both made by a conventional catalyst), when cast, results in a unique film which has significantly improved hot tack strength, good processability (does not adhere to the processing equipment) and will bond by coextrusion or xtrusion lamination to a high density polyethylene substrate in

a laminar structure without the need for an adhesive to achieve such bonding.

The properties of Duraflex® PBO110 and AFFINITY PL1845 are listed in TABLE II and TABLE III below.

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TABLE II

DURAFLEX® POLYBUTYLENE 0110

TY	PICAL PHY	TYPICAL PHYSICAL PROPERTIES*	RTIES*		
		Eng]	English	English	sh
Property	ASTM	:		7.0	
	Test	Unit	Value	ONIC	value
	Method				
General properties				•	
Welt Index	D 1238	1		gms/10 min	0.4
Density	D 1505	1b/ft³	58.0	g/cm³	.915
Mechanical properties					
Tensile strength at yield	D 638	psi	2500	MPa	17.2
Tensile strength at break	D 638	psi	>4000	MPa	>27.6
Flondation at break	D 638	0/0	>300	4 6	>300
	D 638	psi	42500	MPa	293
ശ	D 2240	D Scale	D 60	D Scale	D 60
Thermal properties				. !	1
Melting point range	DTA	ís.	225-229	ပ ·	124-126
Softening point vicat	D 1525	Œ,	235	ပ ပ	113
Coefficient of expansion	D 696	In/in F	7.1 × 10 ⁻³	cm/cm/ c	1.3x10 ⁻
Thermal conductivity	C 177	Btn/ft/		Kcal/m/hr/	
(70 F) (21 C)		Hr/ F/in	1.25	C/cm	16
(/O E) (2 T C)		, , , , , , , , , , , , , , , , , , , ,			

<u>ပ</u> *Compression molded specimen conditioned, 10 days at 73°F (22.8

TABLE III
AFFINITY PL1845
Polyolefin Plastomer

[Physical Properties	Test	Values
	Method	
Percent Comonomer, octene	Dow ²	9.5
Melt Index, dg/min	ASTM D-1238	3.5
Density, gm/cc	ASTM D-792	.910
DSC Melting Point, F(C)	Dow	217 (103)
Dow Rheology Index (DRI)	Dow	1.4
Cast Film Properties, 1.0 mil (25.4 microns	• (
Puncture Resistance, ft-lb/in'(J/cm')	Dow	218 (18)
Dart Impact, g (Method B)	ASTM D-1709	470
rf Tear Strength, g	ASTM D-1709	178
(Type A)	ASTM D-1922	362
Tensile, psi (MPa)	ASTM D-882	580
CD	ASTM D-882	4,847 (33.4)
Ultimate Elongation, % MD	ASTM D-882	527
යා	ASTM D-882	664
Clarity	ASTM D-1746	75
Gloss, 20	ASTM D-2457	145
Haze, \$	ASTM D-1003	0.7
Seal Initiation Temp. F (C)	Dow	210 (99)
These are typical properties only and are not to be regarded as	not to be regarde	d as sales
gpecifications.		
Based on ASTM D-2238, Method B.		
alue based on complex	ity that expresse	s the relative
ng chain branching on	trudability of ho	the extrudability of homogeneous (single
site catalyst) polyolefins.	•	
cast film extruded at 525 F (274 C), 20 mil (0.5 mm) die gap.	l (0.5 mm) die ga	å
Temperature at which 2 lb/in (8.9N/25.4 mi	crons) heat seal	strength is achieved.

ILLUSTRATIVE EMBODIMENT II (Prophetic)

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Blends would be prepared by dry blending in a tumbler mixer the following three ingredients; (i) DuPont Alathon 3159 ethylene-vinyl acetate copolymer (EVA) available from the DuPont Company in Wilmington, Delaware, (ii) Affinity PL1845, an ethylene-octene copolymer of a density of about .910 gm/cc (ASTM D-1238) made by metallocene, available from Dow Chemical Company, and (iii) Duraflex® PB0110 poly-1-butene homopolymer, available from Shell Chemical Company, Houston, Texas, having a melt index of about 0.4 dg/min. (ASTM method D-1238 condition "E") and a The resultant blends are each to be density of about 0.9. coextruded with Hoechst-Celanese 7740 high density polyethylene (HDPE) at a die temperature of about 210°C. into films of about 2.5 mils in thickness using a flat die. The films each would comprise 2.0 mils of HDPE and 0.5 mils of the remaining components. Hot tack strengths are to be tested. Film samples of each composition of one inch wide and 12 inches long are to be tested at temperatures of 90, 100, 110, 120 and 130 °C. Hot tack strengths are to be determined using a DTC Hot Tack Tester using 40 psi seal bar pressure, 150 mm/sec peel speed, 0.5 seconds dwell time and 0.3 seconds delay time setting.

The films which would be made from various blends of this Embodiment and the control (PB and EVA) would be tested for hot tack strength in Newtons per inch at sealing temperatures of 90, 100. 110, 120, and 130°C. It would be unexpectedly found metallocene-made polyethylene, addition of a the that specifically AFFINITY PL 1845 (an ethylene-octene low density copolymer made by metallocene), to a blend of polybutylene and polyethylene vinyl acetate, when cast, would result in a unique film having significantly improved hot tack strength, good processability (does not adhere to the processing equipment) and would bond by coextrusion or extrusion lamination to a high density polyethylene substrate in a laminar structure without the need for an adhesive to achieve such bonding.

The ranges and limitations provided in the instant specification and claims are those which are believed to particularly point out and distinctly claim the instant

inv ntion. It is, however, understood that other ranges and limitations that perform substantially the same function in substantially the same manner to obtain the same or substantially the same result are intended to be within the scope of the instant invention as defined by the instant specification and claims.

CLAIMS

- 1. A packaging film or sheet, capable of forming peel seals suitable for v rtical form/fill/seal packaging, which is made from a blend comprising:
- (i) from about 15 wt.% to about 85 wt.% of an ethylene polymer made by a conventional catalyst;
- (ii) from about 10 wt.% to about 70 wt.% of a metallocenemade polyethylene;
 and
- 10 (iii) from about 5 wt.% to about 55 wt.% of a butene-1 homopolymer or copolymer, based on the total weight of said blend.
 - 2. The film or sheet as described in claim 1, wherein the peel seal strength of said film or sheet is from about 0.5 to about 8.0 pound per inch, and the hot tack strength is from 1.0 to about 4.0 Newton/15 mm.
 - 3. The blend as described in claim 1, wherein said ethylene polymer is polyethylene made by a Ziegler-Natta catalyst.
 - 4. The blend as described in claim 1, wherein said ethylene polymer is an ethylene unsaturated ester copolymer.
 - 5. The blend as described in claim 3, wherein said ethylene polymer is a LDPE, and said metallocene-made polyethylene is an ethylene-octene polymer.
- 6. The blend as described in claim 4, wherein said ethylene polymer is an ethylene-vinyl acetate copolymer, and said metallocene-made polyethylene is an ethylene-octene polymer.
 - 7. A laminate structure suitable for vertical form/fill/seal packaging comprising a backing material to which is bonded a film or sheet, capable of forming peel seals, which is made from a blend comprising:
 - (i) from about 15 wt.% to about 85 wt.% of an ethylene polymer made by a conventional Catalyst;
 - (ii) from about 10 wt.% to about 70 wt.% of a metallocenemade polyethylene;
- 35 and

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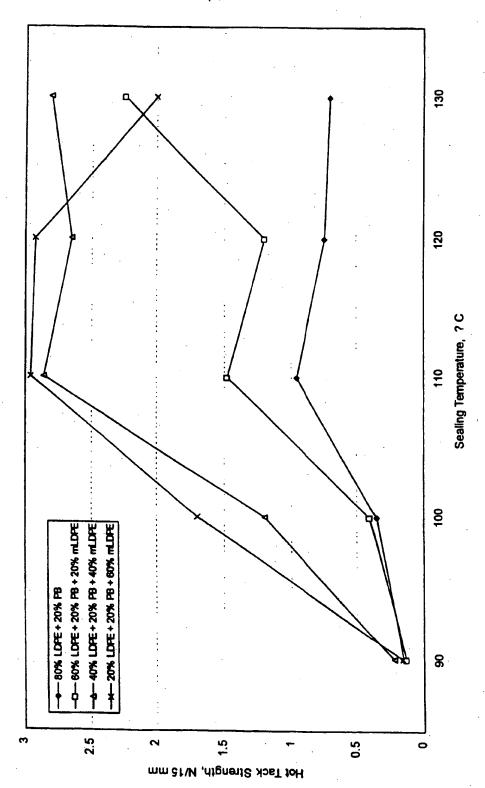
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(iii) from about 5 wt.% to about 55 wt.% of a butene-1 homopolymer or copolymer; based on the total weight of said blend.

- 8. The laminate as described in claim 7, wherein the peel seal strength of said film or sheet is from about 0.5 to about 8.0 pound per inch, and the hot tack strength is from 1.0 to about 4.0 Newton/15 mm.
- 9. The laminate as described in claim 8, wherein said ethylene polymer is a LDPE, made by a Ziegler-Natta catalyst, and said metallocene-made polyethylene is an ethylene-octene polymer.

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10. The laminate as described in claim 8, wherein said ethylene polymer is an ethylene-vinyl acetate copolymer made by a Ziegler-Natta catalyst, and said metallocene-made polyethylene is an ethylene-octene polymer.



SUBSTITUTE SHEET (RULE 26)

INTERNATIONAL SEARCH REPORT

nternational Application No PCT/US 98/27709

A. CLASSII IPC 6	FICATION OF SUBJECT MATTER CO8L23/16 CO8J5/18				
According to) International Patent Classification (IPC) or to both national classifica	tion and IPC			
	SEARCHED				
Minimum do IPC 6	cumentation searched (classification system followed by classificatio ${\tt C08L} - {\tt C08J}$	n symbols)			
Documental	ion searched other than minimum documentation to the extent that su	ich documents are included in the fields sea	rched		
Electronic d	ata base consulted during the international search (name of data bas	e and, where practical, search terms used)			
C. DOCUM	ENTS CONSIDERED TO BE RELEVANT				
Category *	Citation of document, with indication, where appropriate, of the rele	vant passages	Relevant to dalm No.		
X	WO 97 28960 A (TREDEGAR IND INC) 14 August 1997 see page 9, line 22; example 3; t	able 1	1,2,4, 6-8,10		
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1					
Furt	her documents are listed in the continuation of box C.	X Patent family members are listed in	n annex.		
"A" docum	ent defining the general state of the art which is not dered to be of particular relevance	"T" later document published after the inter or priority date and not in conflict with t cited to understand the principle or the invention	he application but ory underlying the		
filing of the filling	ent which may throw doubts on priority claim(s) or i is cited to establish the publication date of another	"X" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is taken alone "Y" document of particular relevance; the claimed invention			
"O" docum	on or other special reason (as specified) ment referring to an oral disclosure, use, exhibition or means	cannot be considered to involve an inv document is combined with one or mo mente, such combination being obviou in the art.	entive step when the re other such docu-		
"P" docum	ent published prior to the international filling date but than the priority date claimed	In the art. "&" document member of the same patent family			
Date of the	actual completion of the international search	Date of mailing of the international sea	rch report		
1	0 May 1999	28/05/1999			
Name and	mailing address of the ISA European Patent Office, P.B. 5818 Patentiaan 2	Authorized officer			
	NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Tx. 31 651 epo nl, Fax: (+31-70) 340-3016	Schmidt, H	·		

INTERNATIONAL SEARCH REPORT

information on patent family members

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